

Shoalhaven Starches Pty Ltd

Shoalhaven Starches expansion project - Modification 11 and Modification 12 (Project Approval MP_06_0228) Revised odour and air quality assessment

May 2017

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1. Introduction

GHD was engaged by Shoalhaven Starches Pty Ltd (Manildra) to conduct an air quality and odour impact assessment for a proposed modification to the approved Shoalhaven Starches Expansion Project (SSEP). The existing Shoalhaven Starches factory is located at Bolong Road in Bomaderry, New South Wales.

Flour and grains are processed at the factory to produce ethanol, starch, gluten, glucose and distiller's dried grain (DDG). Shoalhaven Starches is the holder of Environment Protection Licence number 883 issued for the plant by the NSW EPA.

The Shoalhaven Starches Bomaderry plant currently produces around 225 million litres (ML) of ethanol per year. On 28 January 2009 the (then) Minister for Planning issued Project Approval MP 06_0228 for the Shoalhaven Starches Expansion Project. The Project Approval for the SSEP enabled Shoalhaven Starches, subject to certain conditions, to increase ethanol production in a staged manner at its Bomaderry Plant from the previous approved level of 126 million litres per year to 300 million litres per year. Following the Minister's determination Shoalhaven Starches have been implementing and commissioning works in accordance with this approval. Work on the change in operations has been completed, coupled to quarterly testing (independent audits) of emissions from licensed discharge points (a condition of the Licence), with the purpose to validate the predicted impacts against the original predictions in 2008 for the ethanol expansion.

The increase in ethanol production associated with the SSEP Project Approval was made in response to the NSW Government's ethanol mandate which increased the mandated ethanol content by volume in petrol in NSW from 2% to 6% in October 2011. The SSEP sought to increase ethanol production capacity at the Shoalhaven Starches site to meet the expected increase in demand for ethanol arising from this site. The increase in ethanol production required upgrades to the Stillage Recovery Plant including six additional Dried Distillers Grains Syrup (DDGS) dryers.

Demand for ethanol however has not met that which was anticipated following the introduction of the NSW Governments ethanol mandate. Under these circumstances, it is now proposed to reduce the number of approved DDGS Dryers from six to four (Mod 11). The reduction in Dryer footprint on the site will release land for other development purposes. In addition to the proposed reduction in number of DDGS dryers from six to four, the modification process (Mod 11) also includes the following:

- A minor modification to footprint of the four DDG dryers
- Relocation of the cooling towers in the DDG Plant
- A Mill Feed Silo and structure to feed DDG dryers
- Expanded use of the existing coal and woodchip storage area within the SS Environmental farm
- The addition of two biofilters to cope with the increased number of DDG Dryers
- A forklift maintenance building adjacent to the relocated DDG dryers, along with a container preparation area adjacent to the relocated DDG Dryers

The assessment has also been updated to include additional changes associated with modification application MP06_0028 for the proposed modification to Beverage Grade Ethanol Distillery Plant (Mod 12). Shoalhaven Starches intend to undertake modifications to the existing Ethanol Distillery Plant at their Bomaderry plant to:

- increase the proportion of 'beverage" grade ethanol that is able to be produced on the site. This
 modification will enable increased flexibility in terms of the range of types of ethanol produced at
 the site (i.e. between fuel, industrial and beverage grade ethanol) to meet market demands; and
- to modify the type and location of the Water Balance Recovery Evaporator that has been previously approved under MOD 2 adjacent to the Ethanol Plant

A review of the MP06_0028 Proposed Beverage Grade Ethanol Modification found that the only additional source of odour is the washing column D500 vent which is located on the vacuum column.

These changes, in turn, require an application to EPA accompanied by a report assessing the change (if any) to the predicted off-site impacts. In order to meet EPA NSW requirements outlined in an email from Stefan Press on 4 March 2016; and in an email from Deana Burn (Department of Planning and Environment) on 12 January 2016, this report provides:

- A comparative analysis of the odour results/modelling resulting from the proposed modifications, compared with the odour impacts predicted in the original Air Quality Assessment for the Shoalhaven Starches Expansion Project.
- A comparison of odour results/modelling from the proposed modifications, with the odour results/modelling obtained from the most recent independent odour audits for the premises.
- Where necessary, details of all reasonable and feasible measures to mitigate odour impacts to a level of impact no greater than predicted in the original EA.
- An air quality assessment to demonstrate that the two new biofilters (to treat the DDG driers) will be sufficiently sized to adequately treat the volume and strength of odorous airstreams associated with the modified DDG dryers.

Additional correspondence was provided from the EPA in a letter to Department of Planning and Environment dated 16 February 2017 based on EPA's review of the May 2016 version of this report. This current version has been updated to address these comments Table 1 details the specific issues raised by the EPA and how these matters have been addressed in the body of this revised report.

| EPA issue | Response |
|---|--|
| Odour dispersion modelling was undertaken using average odour emissions data, not the peak | Odour dispersion modelling has been updated using the peak odour emission rates from the odour monitoring conducted by SEMA between May 2016 and February 2017 (four quarters) for EPA ID sources and scaled to a 300 ML per year production. Refer Section 6.1.2 of this report. |
| Odour dispersion modelling is undertaken using monitoring data (based on 219 ML plant capacity), not the approved 300 ML ethanol plant capacity | Odour dispersion modelling has been undertaken for the approved 300 ML plant capacity. Odour emissions for relevant sources have been scaled appropriately and shown in Table 6. |
| Emissions in 2016 are estimated to be approximately 10% less than those in 2008, however, | The revised assessment found that emissions are estimated to be approximately 12% less than those in 2008, and odour impacts are predicted to remain similar at receptors. While there has been overall reductions |

Table 1Response to EPA issues 2017

| odour impacts at receptors are predicted to increase | there has been increases in odour emissions from Gluten dryer 3 and 4, which together make up 32% of the Scenario 1 total. These two sources are modelled as horizontal discharges with a velocity of 0.1 m/s, which contributes to poor odour dispersion. Refer Section 6.2 |
|---|--|
| Unclear as to why receptor heights were changed | Receptor heights in this revised assessment are the same as the original 2008 assessment. This is discussed in Section 7.1 |
| Errors in the emissions for No. 3 starch dryer and No. 5 starch dryer should be revised and remodelled | The emissions inventory and dispersion model have been updated to fix this error. Refer to the updated emissions inventory in Table 6. |
| Difficult to compare emission inventories between GHD (2008) and GHD (2016) | A clear comparison of the emission inventories between GHD (2008) and the inventory in this assessment is provided in Table 6. This also includes comments to explain why there are differences. |
| Odour impacts should be reported in integers, not as decimals | Odour impacts are reported as integers in Table 7. |
| No additional controls are proposed to mitigate the increased odour impacts | An odour mitigation scenario has been assessed in Section 6.3 to reduce odour impacts from the site. |

The revised odour assessment provided in this report is a Level 2 assessment as defined in the DEC Modelling Guideline₁ (ie "refined dispersion modelling technique using site-specific input data"). The Technical framework is used by the Department of Planning and Environment and NSW EPA to assess proposals and set licence and consent conditions, under the *Environment Planning and Assessment Act 1979*, the *Protection of the Environment Act 1997*, and the *Local Government Act 1993*.

It should be noted that some new odour sources in the proposed Packing plant and the Flour Mill areas have been characterised by others² (in terms of source dimensions and odour emission rate) and these have been adopted by GHD in this modelling).

The revised air quality and odour assessment is based on previous site visits, measured and estimated odour emission rates at the site, emission rate databases, an examination of local meteorology, and the outputs of odour dispersion modelling using CALMET/CALPUFF models.

The assessment has been conducted with reference to:

- Approved Methods and Guidance for the Modelling and Assessment of Air Pollutants in New South Wales (EPA, 2016)
- Assessment and Management of Odour from Stationary Sources in New South Wales (Department of Environment and Conservation, 2006).

¹ DEC 2005 "Approved Methods for the Modelling and Assessment of Air Pollutants in New South Wales", 26 August 2005.

² Stephenson Environmental Management Australia (SEMA)

1.1 Scope

The scope of work adopted to conduct the assessment is listed below.

- 1. Check the previous odour emission inventory to confirm if more recent emission rate measurements have been conducted at any identified source.
- 2. Check any source measurements of Total Suspended Particulates (TSP) available from significant dust sources. Assess whether the current TSP inventory is adequate to represent plant emissions of TSP.
- 3. Alter the coordinates of sources to be moved arising from the proposed modification and create new sources (coordinates, emission rates) for the two additional bio-filters. Set the emission rate of sources to be removed to zero.
- 4. Check the performance of the existing biofilters as a guide for the efficiency of the proposed additional biofilters
- Check the proposed changes arising from the proposed plant modification to identify where the built form array of the plant will change and make the required changes in BPIP (a program that assesses the influence of building wakes on air dispersion of nearby sources).
- 6. Conduct the simulations of off-site impact from plant emissions of odour and TSP.
- 7. Report the results for presentation to the NSW Department of Planning and Environment.

1.2 Limitations

This report: has been prepared by GHD for Shoalhaven Starches Pty Ltd and may only be used and relied on by Shoalhaven Starches Pty Ltd for the purpose agreed between GHD and the Shoalhaven Starches Pty Ltd as set out in section 1 of this report.

GHD otherwise disclaims responsibility to any person other than Shoalhaven Starches Pty Ltd arising in connection with this report. GHD also excludes implied warranties and conditions, to the extent legally permissible.

The services undertaken by GHD in connection with preparing this report were limited to those specifically detailed in the report and are subject to the scope limitations set out in the report.

The opinions, conclusions and any recommendations in this report are based on conditions encountered and information reviewed at the date of preparation of the report. GHD has no responsibility or obligation to update this report to account for events or changes occurring subsequent to the date that the report was prepared.

GHD has not been involved in the preparation of the planning submission and has had no contribution to, or review of the submission. GHD shall not be liable to any person for any error in, omission from, or false or misleading statement in, any other part of the submission.

The opinions, conclusions and any recommendations in this report are based on explicit assumptions made by GHD, described in section 1.3 and throughout the body of this document, and limitations of the modelling software CALPUFF. GHD disclaims liability arising from any of the assumptions being incorrect. GHD has prepared this report on the basis of information provided by Shoalhaven Starches Pty Ltd and others who provided information to GHD (including Government authorities), which GHD has not independently verified or checked beyond the agreed scope of work. GHD does not accept liability in connection with such unverified information, including errors and omissions in the report which were caused by errors or omissions in that information.

1.3 Assumptions

The major assumptions used in this assessment are as follows:

- Stack emission testing reports from the past year are accurate and representative of normal operations, and do not vary significantly.
- The odour dispersion modelling using the NSW EPA and US EPA approved regulatory Gaussian puff dispersion model CALPUFF V 5, which was considered appropriate for the location. Limitations with the predicted odour are inherent within the model and in its ability to handle multiple buildings and stacks in a complex setup, with wake effects included. As such, the layout of the plant was simplified in order for the model to handle the setup.
- Odour emissions from the major sources of odour were modelled as both variable emission and fixed point, volume and area sources in CALPUFF with appropriate dispersion characteristics.
- The site representative meteorological data was obtained from previous assessments of the plant, which have been approved by EPA NSW in the past and evaluated against the most recent observations from Nowra in Section 6.
- Small silos in the Packing Plant are conservatively assumed to be filled 24 hours a day.
- Odour sources with horizontal releases have conservatively been modelled with vertical velocities of 0.1 m/s.
- The VOC concentration in the biofilter exhaust is not high enough to induce density flows of the exhaust plume in ambient air.
- The emissions inventory, and therefore the dispersion modelling results, is largely based on estimates and on data measured on site by Stephenson Environmental Management Australia (SEMA). Actual measurements are dependent on site conditions at the time of measurement and these conditions may change. GHD does not accept any responsibility for updating the measurements or estimates made by SEMA.

1.4 Report structure

This report:

- Describes the operations of the plant
- Describes the site-representative meteorological data
- Describes the proposed modifications
- Characterises odour sources at the plant, accounting for the required changes to the original model setup in 2008
- Presents the results of odour dispersion modelling for the existing and proposed scenarios using CALPUFF
- Presents a summary of the results and draws conclusions as to the off-site impacts (both odour and dust)
- Outlines the limitations of the analyses and conclusions presented.

2. Site location and context

2.1 Site description

Figure 1 shows the location and layout of the Shoalhaven Starches plant in Bomaderry, New South Wales. It is located between the Shoalhaven River and township of Bomaderry. The plant comprises a factory, a proposed (but not yet constructed) packing plant and environmental farm. The packing plant lies immediately to the north of the factory, while the environmental farm is situated approximately 400 m to the east.

Nearby Rural Residences

The site is proximate to a number of sensitive receptors. The township of Bomaderry lies to the northwest of the factory and west of the packing plant. Nowra is situated south of the plant. The nearest receptors to the factory, packing plant and environmental farm are identified in Figure 2, with the approximate distances and orientation of each residence from the plant listed in Table 2. These receptors were selected to be consistent with previous odour assessments of the plant. These residences qualify as sensitive receptors, as defined in the DEC odour assessment guideline as "a location where people are likely to work or reside; this may include a dwelling, school, hospital, office or public recreational area" (Department of Environment and Conservation, 2006).

| Receptor | Range, m | To nearest odour source | Direction | Easting (m) | Northing (m) |
|----------|----------|----------------------------|-----------|-------------|--------------|
| R1 | 150 | Packing Plant | W | 281,430 | 6140,610 |
| R2 | 1300 | Factory | SW | 280,400 | 6139,650 |
| R3 | 700 | Factory | S | 281,510 | 6139,310 |
| R4 | 1300 | Factory | SE | 283,000 | 6139,450 |

Table 2Location of identified sensitive receptors





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3. Operation description

3.1 General overview

Wheat flour and grains (wheat) are processed at the Shoalhaven Starches factory to produce ethanol, starch, gluten and glucose. Solid wastes are treated to produce distiller's dried grain (DDG), with liquid wastes being transferred to the environmental farm waste water treatment plant. Excess treated waste water is irrigated onto pasture. The main processing and materials treatment areas at Shoalhaven Starches comprise the:

- Flour mill
- Starch plant
- Glucose plant
- Ethanol and distillation plants
- DDG plant
- Packing plant
- Pellet Plant
- Environmental farm

A brief description of the production process associated (including emission control) with each plant is given below. Figure 3 shows the layout of the plant in terms of its operational areas, along with the major odour sources of the plant, accounting for around 80% of total odour emissions (excluding the environmental farm).

3.2 Flour mill

Shoalhaven Starches commenced full operations at the flour mill in June 2011. The flour mill was originally approved by NSW Department of Planning and Environment in 2007 and was consolidated into the ethanol expansion project approval in 2008.

Proposed modifications to the flour mill were approved in March 2016, which enabled an increase in the total flour production capacity on the site from the previously approved limit of 265,000 tonnes per annum to 400,000 tonnes per annum. The overall amount of flour used in the production process at the Bomaderry site will however remain within the previously approved 20,000 tonnes per week limit.

The flour is used in the plant to produce starch, gluten, glucose and ethanol. All remaining mill feed and pollard (flour sieving rejects) is processed through the DDG dryers for sale as stock feed. Flours from the various grinding operations are collected and blended together before passing through final treatment and weighing operations to bulk storage bins. Flour is taken from these bins for use in existing site production processes.

All air extracted from the mill is passed through Buhler Airjet bag houses prior to being discharged to the atmosphere vertically via four individual stacks. Approval has previously been obtained for the installation of additional plant to increase production, along with two additional exhausts from the roof of the building.

Flour mill stack testing was last conducted in September 2011 by SEMA, for both TSP, PM_{10} and odour.

3.3 Starch plant

Within the starch plant, flour is processed to separate the starch from gluten (the protein component of flour). The starch is graded, dried and packed for shipment. Different grades of starch are manufactured for food and paper making applications. Starch that is not used for these applications is used as a raw material for the ethanol plant. Gluten is dried and sold for use in the food industry.

Aqueous (water-based) wastes are reused within the plant or are transferred to the environmental farm waste water treatment plant.

Starch Dryer No.5 has been constructed and is undergoing commissioning (see Figure 3). No change to the production volume is predicted.

3.4 Glucose plant

The glucose plant (contained within the starch plant area) houses two lines; the 'confectioners' glucose line and the 'brewers' glucose line. Confectioner's glucose is distinguished by having been demineralised to remove latent odours and flavours that might be carried through to the final product by the glucose.

Both processes use starch as the raw material. The starch is broken down to its constituent glucose molecules using enzymatic and hydrolytic processes. Water is removed from the resulting solutions using evaporation to produce glucose and brewer's solutions of desired concentration. The glucose product is shipped to customers in bulk containers.

The glucose manufacturing process generates aqueous wastes, mostly condensate from the evaporators, which is reused during regeneration of the ion exchangers.

3.5 Ethanol and distillation plants

Waste starch from the starch plant is transferred to the ethanol plant and fermented to produce ethanol. Starch (described in section 3.3), which is in suspension, is heated in jet cookers before being fermented.

Fermentation is carried out in fermentation vessels using the treated substrate to which an ethanol-producing yeast inoculum has been added. The yeast inoculum is generated using yeast propagator vessels, these being seeded using commercial strains of yeast.

Wastes from the fermenters are transferred to the DDG plant (refer to section 3.2) for processing. Fermentation liquor from the ethanol plant is transferred to the distillation plant where water and other impurities are removed to produce various grades of ethanol.

3.6 DDG plant

Wastes from the ethanol and distillation plant are dewatered in decanter centrifuges and dried in steam dryers to produce granular DDG. Light phase from the DDG decanters is evaporated to recover soluble protein (syrup) and produce clear condensate (liquid line). The syrup is added to the dryer feed for recovery of the solids (solids line). DDG granular product is transferred to the DDG Pellet Plant for pelletising; the DDG pellets are stored in silos. Some of the granular DDG product is stored in a storage shed until it is loaded into trucks in the DDG load-out area.

Exhaust gases from the existing DDG dryers (three) are transferred to the boiler air intake in order to destroy odorous components of the gases by combustion.

3.7 Steam production

Steam is generated at Shoalhaven Starches by four gas fired boilers (numbers 1, 3, 4 and 7), one wood fired boiler (number 2) and two coal fired boilers (numbers 5 and 6) boilers. The combustion gases from these boilers are discharged via stacks, with boilers 5 and 6 having a combined stack. Exhaust from boiler 4 is treated in a cyclone and those from boilers 5 and 6 are treated in a bag house prior to discharge to atmosphere.

3.8 Environmental farm

A number of wastewater streams are produced at the factory. These consist of five clear condensate streams (distillation plant condensate, evaporator condensate, DDG condensate, a small flow from the carbon dioxide plant and boiler blowdown) and a combined 'dirty' stream from the factory processes. The 'dirty' wastewater streams are combined in the farm tank (located at the factory) and pumped to the waste water treatment plant. Treated water is pumped back to the factory for re-use, while excess treated water is stored in dams for irrigation on the farm.

3.9 Packing plant (proposed)

It is proposed that dried gluten/starch will be pneumatically transferred from the existing site to the proposed new packing plant via underground pipes. This dried material is proposed to be stored in silos.

At present, the approved packing plant has not been constructed at the Shoalhaven Starches sites. The proposed packing plant was assessed by SEMA in 2015 (Stephenson Environmental Management Australia, 2015).

The packing plant will consist of seven silos that will store either gluten or starch product. The medium and large silos are to be filled 24 hours a day, seven days a week, while the small silos can be filled at any time of the day for eight hours.

3.10 Other activities

3.10.1 Product load-out areas

Starch, glucose and ethanol products are loaded into road tankers from bulk storage silos and tanks. Load out of starch and glucose does not have the potential to generate odours, as these products have a low inherent odour characteristic.

Given the flammable nature of ethanol, the load out process is strictly controlled for occupational health and safety purposes. These controls have the secondary effects of minimising the potential for vapour generation and spillage.

3.10.2 Cooling towers

Cooling towers operate as part of the cooling water circuit for the ethanol glucose and DDG plants. The recirculated cooling water has the potential to absorb odours and to disperse the odours to atmosphere during the evaporative cooling (aeration) process within the cooling towers. In addition, contamination of the cooling water by-product, process intermediates or wastes can introduce odorous materials direct to the cooling water, which can greatly increase its odour generating potential. The aeration process readily strips the more volatile (and potentially odorous) compounds from the water, providing a high-volume potential source of odour that is released direct to atmosphere.

3.10.3 Biofilters

Exhaust air from odorous sources at the DDG plant is captured and ducted to two existing soilbed biofilters, each having a surface area of 110 m², located at the southwest corner of the factory (on the southern margin of the container storage area – placed to the left lower margin in Figure 3). The biofilters comprise a bed of organic bark and compost material (the matrix), with distribution of the odorous airstream through the floor of the biofilter via a manifold. Biological oxidation of odorous compounds takes place as the foul air percolates upward through the matrix. The oxidation is achieved by a population of microorganisms in the bed.

While the efficiency of biofilters destroying odorous components of the waste air varies according to a range of factors including soil moisture, composition and temperature, it is very high. Any odour in the exhaust air from the biofilter is due to the inherent odour of the matrix materials and typically has an 'earthy' characteristic. The odour level of the matrix is typically in the range of 250 to 500 OU, and it is this 'background' level that limits the efficiency of a soilbed biofilter.

The two biofilters at the site operate in parallel and are sized so that one biofilter can be taken offline during periodic replacement of the matrix of the sister filter.

As such, a soilbed biofilter operating as designed, with no malfunctions, will not vary significantly in its odour emissions; it will emit at the matrix background level independent of fluctuations in the input odour loading.

3.11 Proposed modifications

Manildra propose to change the configuration of the DDG Plant to the southwest of the factory site. These changes are shown in Figure 4 and consist of a staging process, and thus impacts have been assessed separately.

Proposed modifications to the ethanol distillery (Mod 12) are shown in Figure 5 and includes:

- Relocation of previously approved Evaporator;
- Beverage grade ethanol plant. Existing structures (two water tanks, diesel above ground tanks, a brick pump house, and redundant former plant) will be demolished as part of these works;
- Installation of three above ground tanks. Two 400 kL tanks (tanks 1 and 2) will be installed in the ethanol recovery area. An existing tank will be removed to make room for one of these tanks. A 1,000 kL tank (tank 8) will be installed in the ethanol storage area;
- Cooling towers;
- New gantry pipe connecting the ethanol plant, tanks and cooling towers;
- Electrical substation;
- Emergency ISO tank container storage area, including extension of an access road (as shown in red) from the former Dairy Farmers complex;
- An internal access road to and from the ISO tank container storage; and
- Two railway sidings will be extended along the south-eastern side of a former Dairy Farmers site to accommodate an extension of the railway siding, existing water treatment tanks, pump house and piping will be removed, and existing water treatment ponds will be filled in.
- Proposed car parking area near the existing BOC gas facility.

The main changes affecting odour impacts and dust consist of:

- Scenario 1
 - Installation of DDG dryer 4 to the new building to the north of the proposed container storage area, with air leakage to be collected and ducted to the existing biofilters
 - The installation of three DDG dryers to be ducted to two new biofilters
 - The relocation of the approved cooling towers
 - washing column D500 which is located on the vacuum column (proposed beverage grade ethanol plant)

Further discussion of this scenario is presented in section 6.1.2.





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Figure 4 Proposed changes to DDG plant



Figure 5 Proposed changes to beverage grade ethanol plans



4. Criteria for assessment

4.1 Odour

Odour Concentration

Odour 'strength' or concentration is measured in odour units (OU), where 1 OU represents the concentration of a sample that can just be detected by 50% of people in a controlled situation where there is no background 'ambient ' odour.

Measurement of Odour

The most common method of measuring odour concentration is Dynamic Olfactometry using the 'forced choice' method. Dynamic olfactometry simply dilutes the odour sample in known ratios with odour free air. At each dilution, the diluted odour and a zero odour is presented in turn to six panellists via two 'sniffing' ports. Further, the selection of the port with the diluted odour sample is randomly reassigned at each presentation. Each panellist is required (forced) to nominate the port (left or right) from which the diluted odour emanates. Each panellist's response (i.e. 'guess', 'likely' or 'certain') is recorded. The sequence of presentations generally follows a decreasing dilution ratio, and when half of the panellists have correctly returned a 'certain' response, that dilution ratio is numerically equal to the concentration of the original, undiluted odour sample. Hence, for example, if the dilution needed to get the 50% response was 250:1, then by definition the original sample had an odour concentration of 250 OU.

EPA Criterion for Odour

EPA has defined an odour criterion and the Odour Guideline specifies how it should be applied in dispersion modelling to assess the likelihood of nuisance impact arising from the emission of odour.

Odour impact is a subjective experience and has been found to depend on many factors, the most important of which are:

- The Frequency of the exposure
- The Intensity of the odour
- The Duration of the odour episodes
- The Offensiveness of the odour
- The Location of the source

These factors are often referred to as the FIDOL factors.

DEC defined the odour criterion to take account of two of these factors (**F** is set at 99 percentile, **I** is set at from 2 to 7 OU). The choice of criterion odour level has also been made to be dependent on the population of the affected area, and to some extent it could be said that population is a surrogate for location – so that the **L** factor has also been considered. The relationship between the criterion odour level **C** to affected population **P** is given below.

C = **[log P-4.5]÷-0.6**

Equation 1

Table 3 lists the values of C for various values of affected populations as obtained using equation 1.

Table 3 Odour criterion for the assessment of odour

| Population of affected community | Odour performance criteria (nose response odour certainty units at 99 th percentile) |
|----------------------------------|---|
| Single Residence (≤ ~2) | 7 |
| ~ 10 | 6 |
| ~ 30 | 5 |
| ~ 125 | 4 |
| ~ 150 | 3 |
| Urban (~2,000) | 2 |

The NSW Approved Methods specifies a criterion of two odour units at the 99th percentile over a short term averaging nose-response time of one second for a complex mixture of odorous air pollutants in an urban area (population greater than 2000 or with schools and hospitals). The criterion is applied at the location of the nearest sensitive receptor or likely future location of sensitive receptor.

5 OU is commonly taken as a conservative measure of the odour level which can be distinguished against the ambient background level of odour, and which if offensive, could result in complaint.

1 OU generally cannot be detected in a non-laboratory situation (i.e. where the ambient background odour levels reduce the detectability of a given odorant).

As the CALPUFF dispersion model (utilised in this assessment), when operating in micrometeorological mode can only predict concentrations over an averaging period of one hour, a ratio between the one second peak concentration and 60 minute average concentration has been applied to the source odour emission rates. In this manner, the predicted one hour odour levels predicted in CALPUFF represent the corresponding one second short-term levels required to be compared to the DEC criterion. The ratio is known as the peak to mean ratio (PM60). PM60 is a function of source type, stability category and range (i.e. near or far-field), and values are tabulated in the modelling Guideline3. This is reproduced below.

| Source type | Pasquill–Gifford stability class | Near-field P/M60* | Far-field P/M60* |
|-------------------------|-------------------------------------|----------------------|---------------------|
| Area | A, B, C, D | 2.5 | 2.3 |
| | E, F | 2.3 | 1.9 |
| Line | A–F | 6 | 6 |
| Surface wake-free point | A, B, C | 12 | 4 |
| | D, E, F | 25 | 7 |
| Tall wake-free point | A, B, C | 17 | 3 |
| | D, E, F | 35 | 6 |
| Wake-affected point | A–F | 2.3 | 2.3 |
| Volume | A–F | 2.3 | 2.3 |

| Table 6.1: Factors for estimating peak concentrations in flat terrain (Katestone | e |
|--|---|
| Scientific 1995 and 1998) | |

* Ratio of peak 1-second average concentrations to mean 1-hour average concentrations

Figure 6 Extract from NSW Approved Methods

³ Approved Methods for the Modelling and Assessment of Air Pollutants in NSW (DEC, 2005).

4.2 Dust

Dust impacts can be assessed against several criteria, namely:

- Total suspended particles (TSP)
- Deposited dust
- Fine particulate matter less than 10 micron equivalent aerodynamic diameter PM₁₀

Table 4 below summarises the criteria for pollutants relevant to the operation of the plant from the Approved Methods for the Modelling and Assessment of Air Pollutants (EPA, 2016).

Table 4 Air quality impact assessment criteria - other pollutants

| Pollutant | Averaging period | Criterion - |
|-------------------------------------|------------------|---------------------------|
| Particulate Matter PM ₁₀ | 24 hours | 50 μg/m ³ |
| | Annual | 30 µg/m ³ |
| TSP | Annual | 90 μg/m³ |
| Deposited Dust | Annual | 4 g/m ² /month |

5. Meteorological data

A 12-month dataset was constructed using the 3D prognostic modelling package, TAPM and the diagnostic 3D meteorological model, CALMET for the period from January to December 2004. This 12 month period was chosen to be consistent with previous modelling undertaken for the 2008 Air Quality Assessment, approved at the time by EPA and to allow to a direct comparison to previous modelling. Further detail is provided in Appendix A in regards to the selection and construction of the meteorological dataset used in the modelling.

The CALMET modelling can be summarised as follows:

- Prognostic models TAPM and CALMET were used for initial wind field 'guesses'
- Observations from both the environmental farm Automatic Weather Station (AWS) and Nowra AWS were used to optimise and check the prognostic model simulations
- Wind speeds and direction observations from the environmental farm AWS were assimilated into the prognostic model to make the data site-specific

The result of assimilating this data into the CALMET simulations makes the data site-specific (required for a Level 2 assessment), and inter-annual variability is not required to be accounted for, with the conditions of the Approved Methods met for using "*atleast one-year of site-specific meteorological data*".

An annual wind rose generated using CALMET is provided in Figure 7 to show the wind field at the factory. The following trends are evident from Figure 7:

- Annual average wind speed of 3.2 m/s
- Winds are most prevalent from the west and west northwest, accounting for around one third of all winds
- Winds are least prevalent along the north-south axis
- Light winds (shown in grey) are more prevalent from the northwest
- Drainage flows occurring during stable conditions at night time are dominated by the following distinct features (in order of scale):
 - Shoalhaven River running west to east through the site
 - Browns Mountains to the northwest of the site
 - Yalwal State Forest mountain range to the west.



Figure 7 CALMET wind rose for the factory

6. Emission inventory

6.1 Odour

6.1.1 Source identification

Odour emanating from Shoalhaven Starches is comprised of a complex mixture of primarily odorous volatile organic compounds (VOCs). VOC speciation data from a range of principal odour sources indicates that the individual VOCs within the mixture tend to be classified under odour-based air quality criteria rather than toxicity-based⁴ criteria. Therefore, the identified sources of odour are modelled collectively as odour.

Consistent with the 2008 Air Quality Assessment (GHD, 2008), the following sources contribute to the majority of the odour impacts from the Shoalhaven Starches sites, in order of significance:

- Environmental farm (effluent treatment and storage system)
- DDG Plant (including Pellet Plant exhaust stack and biofilters)
- Starch Plant (Gluten and Starch Dryers)
- Ethanol Plant (yeast propagators and retention tank)

A number of other minor odour sources contribute to the remainder of the plant's odour impact. These are detailed in Appendix B.

6.1.2 Proposed modifications

The proposed modifications, as described in section 3.11, are summarised below.

Approved and existing (baseline) operations

The approved and existing operations consists of all odour sources at the Shoalhaven Starches plant, including EPA monitored sources and all minor sources, conservatively scaled for a 300 ML per year production. It also includes approved operations that are sources of odour, both recently constructed. This consists of:

- Silos at the proposed packing plant. The Air Quality Impact Assessment: Modifications to Packing Plant conducted by SEMA (Stephenson Environmental Management Australia, 2015), calculated a maximum modelled odour concentration of 0.7 OU from a combined OER of the silo vents of 1,882 OUm³/s.
- Recent upgrades to the existing flour mill. The Air Quality Impact Assessment: Modifications to Existing Flour Mill conducted by SEMA (Stephenson Environmental Management Australia, 2015) calculated a maximum modelled odour concentration of 0.3 OU from a combined OER of the mill baghouses of 471 OUm³/s.
- Starch Dryer 5, recently constructed in the factory building on Bolong Road near the Maintenance Workshop. The Air Quality Impact Assessment: Dryer 5 Relocation conducted by SEMA (Stephenson Environmental Management Australia, 2015) calculated a maximum modelled odour concentration of 0.54 OU from an increase in OER of 6,800 OU/m³/s associated with Dryer 5.
- Proposed new Flour Mill B. The Air Quality Impact Assessment: Proposed Flour Mill B conducted by SEMA (Stephenson Environmental Management Australia, October 2016)

⁴ Based on VOC speciation data for selected sources in the DDG plant: DDG dryers, palmer cooler and condensate tanks.

calculated a maximum modelled odour concentration of 0.7 OU from a OER of 5637 $OU/^{m3}/s$.

The following assumptions and additions apply to the audit modelling:

- Peak odour emission rates were taken from the odour monitoring conducted by SEMA between May 2016 and February 2017 (four quarters) for EPA ID sources and scaled to a 300 ML per year production. The quarter with the maximum measured total OER was selected for use in the assessment and is consistent with guidance in the Approved Methods and the recommendation from EPA (16 February 2017) that peak emissions should be assessed. The peak period was found to be quarter 3 2016. A summary of these is presented in Appendix C.
- Specific odour emission rates from the effluent storage dams were based on most recent testing (May 2016) in conjunction with historical results
- Odour emission rates were assumed to be unchanged for sources originally measured in 2008 that have not been measured since

New sources:

- Pellet plant exhaust stack, taking odorous air from the pellet coolers, drag chains, container loading/aspiration channel, DDG cyclones and DDG silos
- No. 5 starch dryer
- Seven silos for the new packing plant
- Pellet plant fugitives, consisting of the wheat silos, barley intake fan, barley silo fan, barley grinding fan and bulk bag aspiration fan (non-DDG odour sources)

The installation of one new DDG dryer (DDG dryer 4) and Mill Feed silo, along with the relocation of the eastern cooling towers and the addition of the building to house the dryers (included in the model to update building wake effects).

The installation of an additional three dryers as well as DDG dryer 4, all to be ducted and captured via the two new biofilters. This incorporates the additional sources:

- Western cooling towers adjacent to the new DDG dryer building, assumed to have the same odour emissions and source characteristics as from the existing cooling towers
- Two new biofilters, adjacent to the existing biofilters
- washing column D500 which is located on the vacuum column

At present, two biofilters operate on a combined design air flow of $15,000 \text{ m}^3/\text{h}$, with the flow split between two biofilters, each with a surface area of 110 m^2 . The biofilters receive air from a combination of odorous sources in the existing DDG plant, including feed dump, condensate, finish feed, finisher pump tank, dryer feed tank, feed holding tank and CIP (fresh caustic).

Air leakage from DDG Dryer 4 is to be captured and ducted to the existing biofilter. The air leakage is estimated to be 1500 kg/h at 54°C. At a density of air, this equates to 0.38 m³/s of additional exhaust air to feed to the biofilters. Each biofilter is designed for an air intake/treatment of 15,000 m³/h (4.17 m³/s).

A summary of the existing biofilter operations is provided below in Table 5. As stated in the (The Odour Unit, 2010).

"the odour destruction performance of the biofilter is not dependent to any significant extent on inlet odour concentrations less than 50,000 odour units".

If this odour concentration is exceeded, the surface loading requires an update in the design to cope with the additional odour.

| Parameter | Unit/measure | Parameter |
|---|------------------------|------------------------------|
| Exhaust air flow rate ducted to biofilter (2016/2017) | Flow rate | 2.6 to 3.1 m ³ /s |
| Current total odour emission rate ducted to biofilter (2016/2017) | Odour concentration | 7,600 to 9,800 OU |
| Biofilter A | area | 110 m² (55% split) |
| | Air flow split | 55 % |
| Biofilter B | area | 110 m ² |
| Dioliter B | Air flow split | 45 % |
| May canacity for one biofilter | Flow rate | 15,000 m ³ /hour |
| Max capacity for one biofilter | | 4.17 m ³ /s |
| Bed depth | Length | 1.8 m |
| Contact time | Time | 48 s |
| Spare capacity (at maximum observed flow rate 2016/17) | Flow rate | 3.3 m ³ /s |
| Additional exhaust air from DDG dryer 4 (proposed) | Flow rate | 0.38 m ³ /s |
| Additional exhaust air likely from DDG dryers 5 to 7 (proposed) | Flow rate | Up to 5.0 m ³ /s |

Table 5Summary of biofilter operations

The biofilter design for a bed depth of 1.8 m gives a contact time of 48 seconds – this is considered more than adequate to allow either biofilter to accept double the load while its' sister biofilter is off-line for replacement of the bed matrix.

With the two existing biofilters operating at around 50% of capacity, an additional 0.38 m³/s of exhaust air could be absorbed by the two existing biofilters, resulting in no changes required to connect DDG dryer 4 to the system for Scenario 1.

The addition of DDG dryers 5 to 7 is expected to also involve the addition of numerous decanters and other potential odour sources which are yet to be fully defined. As a result, for this scenario it is assumed that the new system would be equivalent to the existing system for the DDG building and will require an additional two biofilters (with flow splitting) on site.

The flow rate of the new washing column vent will be 70 kg/h of air saturated in water (0.07 m₃/h assuming a density of 1000 kg per m₃) (Technip Technical specification X500 – Vacuum package). This equates to 0.001166 m₃/min of air flow which would have a similar odour character and level to the measured D6 vent. The corresponding OER based on this flowrate is 23.3 ou.m₃/min (~0.4 ou.m₃/s)

6.1.3 Source summary

Existing and Approved (Baseline) scenario

Modelling for the approved baseline scenario comprised the following sources:

- 49 point sources (each assumed at constant OER) throughout the factory area
- Three point sources with variable emissions within the factory area
- 11 area sources (consisting of two biofilters and the effluent treatment ponds)
- Five volume sources within the factory area

Scenario 1

Addition of DDG Dryer 4 and the buildings has the following additional two sources:

- Cooling towers located on the western side of the proposed DDG building, adding an additional 172 OUm³/s, based on measurements from the existing on-site cooling towers to total existing OER from the plant.
- Mill feed silo, located to the south of the existing DDG building, adding an additional 173 OUm³/s, based on measurements from the existing Gluten 1 B silo to total existing OER from the plant.

Addition of DDG dryers 5 to 7 has the following additional sources:

• Two biofilters, located adjacent to the existing biofilters in the southwest corner of the plant, adding an additional 0.85% to total existing OER from the plant (based on doubling the current OER from the two existing biofilters).

Upgrades for modifications to the proposed beverage grade ethanol distillery plant (MP06_0028) has the following additional source:

washing column D500 which is located on the vacuum column

These sources are detailed in Appendix B.

6.2 Comparison of site total odour emissions for nominated Scenarios

A comparison of the sources that were modelled in the 2009 approval of the ethanol expansion project (GHD, 2008) and those that have been modelled as part of the MOD11 proposal (GHD May 2016) and MOD12 have been included below in Table 6. It can be seen that odour levels between 2008 and this assessment decrease by approximately 12%. Source release parameters are shown in more detail in Appendix B.

Although total emissions are lower now than in 2008, predicted impacts as shown in Section 7 (Table 7) of this report are not predicted to change at all when predicted odour units are reported as integers as requested by EPA. This is largely due to increases in odour emissions from Gluten dryer 3 and 4, which together make up 32% of the Scenario 1 total. These two sources are modelled as horizontal discharges with a velocity of 0.1 m/s which contributes to poor odour dispersion. This is discussed in more detail in Section 6.3.

The 12% decrease also the result of measured odours versus 2008 predictions and removal of various odour sources as shown in Table 6.

| Source | Model Reference | 2008 EA MOER ou.m3/s before control | 2008 EA MOER ou.m3/s stage 1 controls | Current 2017 MOER ou.m3/s (Mod 11 and Mod 12) | Comments |
|--------------------------------|--------------------|--|---|---|--|
| Boilerhouse | | | | | |
| Boiler no 2 - wood waste | BOILER2 | 13104 | 13104 | | Odours emanating from the combustion of coal were not included in 2008 modelling (EA 2008 p.34) |
| Boiler no 4 | BOILER4 | 22889 | 22889 | 3171 | Conversion from coal-fired to gas-fired boiler has reduced boiler air flow rates. |
| boiler 5 & 6 | BOILER5 | 72440 | 72440 | 38463 | Original modelling assumed DDG odour destruction efficiency of zero % through boilers (EA 2008 p.34) |
| | | | Sub-total MOER | 41634 | |
| | | | % of Total MOER | 15% | |
| DDG Plant | | | | | |
| Feed dump tank | DDG20 | 8917 | 1338 | | ducted to biofilter |
| Condensate tank | DDG23 | 25711 | 3857 | | ducted to biofilter |
| Vent condenser | DDG24 | 3500 | 525 | | ducted to biofilter |
| Condenser drain | DDG25 | 3167 | 3167 | 31 | Now labelled VCD. Condensate collected via ground level drain and then conveyed via pipe to waste water treatment plant @ farm |
| Finish feed tank | DDG26 | 18333 | 2750 | | ducted to biofilter |
| Finisher pump tank | DDG28 | 1433 | 215 | | ducted to biofilter |
| Dryer feed tank | DDG30 | 1433 | 215 | | ducted to biofilter |
| DDG Syrup Feed holding tank | DDG31 | 1317 | 198 | | ducted to biofilter |
| CIP tank | DDG32 | 417 | 63 | | ducted to biofilter |
| DDG tent storage area | DDG36 | 12862 | 1929 | 1929 | Assumed control was pelletised DDG would reduce odour emissions. |

Table 6 Comparison of odour emissions from 2008 emissions to current proposal

| Product storage sheds | DDG34 | 6820 | 1023 | 1023 | Assumed control was pelletised DDG would reduce odour emissions. |
|------------------------------|-------|-------|------|-------|---|
| Grounds | DDG37 | 203 | 0 | | Assumed control was that pellet plant would prevent any spillage of DDG product in the forecourts areas of DDG storage areas and so reduce odour to zero |
| DDG dryer building | DDG39 | 70504 | 7050 | | Odour sources ducted to boilers |
| palmer cooler | DDG16 | 17666 | 2650 | | Ducted to boilers |
| DDG heat exchanger | DDG45 | 2333 | 0 | | Ducted to boilers |
| Decanter 3&4 | DDG5 | 1700 | 1700 | | Ducted to boilers |
| Decanter 1&2 | DDG2 | 260 | 260 | | Ducted to boilers |
| Decanter feedtank | DDG1 | 217 | 108 | | Ducted to boilers |
| feed dryer baghouses | DDG18 | 867 | 130 | | Ducted to biofilter |
| light phase tank | DDG19 | 450 | 450 | 20 | Ducted to boilers |
| cooling towers | DDG46 | 68333 | 6833 | 172 | Odour testing undertaken has confirmed low results. Also possible condensate used in cooling towers when original testing in 2008 done - this practice no longer occurs |
| DDG Loadout Shed Awning | DDG35 | | | 923 | Not in EA 2008 modelling inventory |
| DDG evap condensate tanks | | 36000 | 5400 | | Not installed (part of proposed 6 DDG dryers) Proposed to be ducted to biofilter. |
| DDG transfer cyclones (6) | | 9083 | 1362 | | Existing cyclones go to boilers 5 & 6. Proposed cyclones to go through to existing and new biofilters |
| DDG dryers (6) | | 6321 | 948 | | Existing DDG dryer (3) go to boilers 5 & 6; proposed new DDG Dryers (4) to go through to existing and new biofilters |
| Decanters (10) | | 8417 | 1263 | | Existing decanters go to Boilers. Proposed new decanters to go through to existing and new biofilters |
| pelletiser baghouse (2) | | 34378 | 5157 | | Transfered to the pelletiser exhaust stack - PPES |
| DDG general ventilation | | 722 | 108 | | Includes proposed DDG evap. condensate tanks and minor point sources associated with Pelletizer plant transfer points (EA 2008 p.32) |
| pellet exhaust stack | PPES | | | 38240 | Installed via MOD 5 |
| Pellet silo | S12 | 350 | 350 | 350 | |
| stillage surge tank | SST | | | 149 | |

| pellet plant fugitives (non-DDG sources) | PPF | | | 5771 | Installed MOD 5 |
|---|-------|-------|--------------------|-------|--|
| Additional Cooling towers | CTP | | | 172 | Proposed MOD11 |
| | | | Sub-total MOER | 48780 | |
| | | | % of Total MOER | 18% | |
| Ethanol Plant | | | | | |
| Grain silo baghouse | E1 | 183 | 183 | | De-commissioned |
| ethanol cooling towers | E23 | 65833 | 0 | | Located in an area away from odour sources. Used fresh water. Odour considered negligible (EA 2008 p.12) |
| Yeast Propagators -tanks 4 and 5 | E15Y4 | 14167 | 14167 | 820 | Now YP45. Reduction due to removal of ammonia addition. 2 Tanks operate in batch sequence. |
| Yeast Propagators -tanks 4 and 5 | E15Y5 | 14167 | 14167 | | Now YP45. Reduction due to removal of ammonia addition. |
| Grain retention tank | E8 | 6500 | 3250 | 3250 | Now labelled GRT. |
| propagator tanks 1,2,3 | E14 | 5500 | 5500 | | Configuration of propagator tanks changed - odour now accounted for via tanks YP45 |
| Ethanol recovery scrubber | ERESC | | | 3132 | |
| Fermenters 10-16 | FERM | 1237 | 1237 | 2668 | Previously sum of FERM10 (518) and FERM11(719) in 2008 |
| jet cooker 1 retention tank | E13 | 1067 | 1067 | 1067 | |
| jet cooker 2/4 grain retention | E7 | 1133 | 1133 | 567 | |
| Feed to distillery | E22 | 167 | 83 | 83 | |
| | | | Sub-total MOER | 11587 | |
| | | | % of Total MOER | 4.2% | |

| Incondensable gases vent | D6 | 400 | 400 | 558 | |
|----------------------------------|------|------|--------------------|------|--|
| Molec. sieve vacuum drum | D2 | 1350 | 1350 | 1350 | |
| DME vent | D12 | 107 | 107 | | De-commissioned |
| Column Washing Vent | CWV | | | 23 | Proposed MOD 12 |
| | | | Sub-total MOER | 1931 | |
| | | | % of Total MOER | 0.7% | |
| Starch and Glucose | | | | | |
| cyclone and FF ID4 | A4 | 1654 | 1654 | 679 | Existing Flour Mill |
| cyclone and FF ID5 | A5 | 617 | 617 | 96 | Existing Flour Mill |
| cyclone and FF ID6 | A6 | 1477 | 1477 | 449 | Existing Flour Mill |
| cyclone and FF ID7 | A7 | 551 | 551 | 932 | Existing Flour Mill |
| Drum vac receiver | C4 | 3500 | 3500 | 1400 | Only 1 drum in operation now, previously 3 in 2008 |
| Dry gluten roof bin | S07 | 4500 | 4500 | 4500 | |
| Enzyme tanks | B7 | 4083 | 2042 | 2042 | |
| flash vessel jet cooker | C1 | | | 970 | |
| flour bin aspirator | S13A | 500 | 500 | 500 | Combined S13 source in 2008 @ 1000 OER (refer to EA 2008 p.30) |
| flourbin aspirator | S13B | 500 | 500 | 500 | |
| flourbin motor drive | S06 | 283 | 283 | 283 | |
| flour mill aspiration (Mod 8) | FMP1 | | | 266 | MOD 8 |
| flour mill aspiration (Mod 8) | FMP2 | | | 205 | MOD 8 |
| high protein dust collector | S08 | 600 | 600 | 600 | |
| ion exchange effluent tank | C18 | 250 | 250 | 250 | |

| no 1 gluten dryer baghouse | S02 | 13182 | 9866 | 5925 | |
|-------------------------------------|-------|-------|--------------------|---------|--|
| no 1 starch dryer | S01 | 6315 | 4736 | 5193 | |
| no 2 gluten/starch dryer | S04 | 5511 | 4133 | 2354 | Result based on gluten drying |
| no 3 gluten dryer baghouse | S03 | 19501 | 14625 | 58917 | High result to be investigated; flow rates highly variable; investigate alternate sampling point |
| no 3 starch dryer | S18 | 6436 | 4827 | 1663 | |
| no 4 gluten dryer baghouse | S05 | 13331 | 9998 | 31222 | High result to be investigated |
| no 4 starch dryer | S19 | 7151 | 5363 | 1824 | |
| no 5 ring dryer gluten/starch | SDR5 | 12881 | 9661 | 4817 | Result based on current gluten drying |
| no 5 starch dryer | SD5 | 6794 | 5096 | 6800 | New starch dryer MOD7 |
| no 6 gluten dryer | GD6 | | | 12568 | |
| no 7 gluten dryer | GD7 | | | 9553 | |
| spray dryer | S20 | 983 | 738 | 738 | |
| starch kestner dryer | DDG40 | 3000 | 0 | | Dryer De-commissioned |
| starch factory rejects | E10 | 183 | 183 | 183 | |
| Farm tank | F18 | 7667 | 3834 | 3834 | |
| pellet mill silo | PMFS | | | 173 | Not constructed MOD10. |
| Flour Mill B Exhaust (10 points) | | | | 5637 | Not constructed MOD10 |
| | | | Sub-total MOER | 165,073 | |
| | | | % of Total MOER | 59% | |
| Packing Plant MOD | | | | | |
| starch silo 1 | PPL1 | | | 86 | Not constructed |
| starch silo 2 | PPL2 | | | 86 | Not constructed |

| gluten silo 1 | PPM1 | | 173 | Not constructed |
|------------------------------|----------------|--------------------|---------|-----------------|
| gluten silo 2 | PPM2 | | 173 | Not constructed |
| gluten silo 3 | PPM3 | | 173 | Not constructed |
| small gluten silo | PPS1 | | 92 | Not constructed |
| small starch silo | PPS2 | | 35 | Not constructed |
| | | Sub-total MOER | 818 | |
| | | % of Total MOER | 0.3% | |
| Area sources: Env fa | arm after WWTP | | | |
| Biofilter A | BIO1 | | 440 | |
| Biofilter B | BIO2 | | 330 | |
| Biofilter C | BIO3 | | 1089 | proposed MOD 11 |
| Biofilter D | BIO4 | | 1280 | proposed MOD 11 |
| storage dam 1 | PO1 | 3600 | 148 | |
| storage dam 2 | PO2 | | 1656 | |
| storage dam 3 | PO3 | | 192 | |
| storage dam 5 | PO5 | | 515 | |
| storage dam 6 | PO6 | | 1775 | |
| SO basin | SOBAS | 23400 | 830 | |
| MBR | MBR | 500 | 62 | |
| | | Sub-total MOER | 8317 | |
| | | % of Total MOER | 3% | |
| Total (2008) | | 317,159 | | |
| Total (Mod 11 and Mod 12) | | | 278,140 | |
| Decrease from 2008 | | | 12 % | |
6.3 Odour mitigation

In order to reduce the potential for odour impacts from the site to meet the odour criterion, a review of significant odour sources was undertaken and how they are released into the atmosphere. The review found that Gluten dryer 3 and 4 which together make up 32% of the site total are horizontal discharges. These were modelled with a velocity of 0.1 m/s, meaning that odour is not being adequately dispersed resulting in elevated ground level odour impacts under certain meteorological conditions. An odour mitigation scenario was designed after consultation with engineers from Shoalhaven Starches.

The following stack discharge scenario has been assessed:

- Gluten Dryer No.3, average airflow velocity of 10.975 m/s, at 65 degrees duct, vertical airflow 9.95 m/s
- Gluten Dryer No.4, average airflow 16.575 m/s, at 45 degrees duct, vertical airflow 11.72 m/s.

Angling the ducts from horizontal towards vertical, enable emissions to be dispersed up into the atmosphere at their calculated velocity. This will assist dispersion of odours and potentially reduce ground level odour impacts.

Results of the odour mitigation assessment are discussed in Section 7.3.

6.4 Dust emissions

6.4.1 Source identification

The main sources of dust, consisting of TSP, PM₁₀ and PM_{2.5}, are listed below:

- Gluten and starch dryers
- Boilers:
 - Boiler 1 Gas fired
 - Boiler 2 Wood fired
 - Boiler 3 Gas fired
 - Boiler 4 Gas fired (converted from coal)
 - Boiler 5/6 Coal fired
 - Boiler 7 Gas fired
- Flour Mill baghouses
- DDG Pellet Plant exhaust stack
- Product silos
- Coal and woodchip stockpiles

No dust emissions are expected to arise from a normal-functioning biofilter, which acts as an impassable filtration device due to the density of its matrix. As a consequence, all new emissions from the proposed DDG dryer 4 (and subsequent DDG dryers 5 to 7) are expected to be captured in the biofilters. No net increase in particulate emissions from the plant as a result of the proposed modifications is therefore predicted. The addition of the cooling towers and mill feed silo are also expected to add negligible particulate emissions to the current footprint of the plant.

The relocation of the coal and wood chip storage area is expected to improve predicted dust impacts caused by wind erosion of unstable/uncovered surfaces. At present, the coal stockpiles

cover an area of approximately 550 m². The relocation of the storage area to the environmental farm north of Bolong Road will increase the distance to sensitive receptors R1 to R4, along with the town of Bomaderry. With appropriate dust controls, including currently used practices of watering and suitable design dimensions, it is predicted that this would result in lower levels of dust due to wind erosion encountered at nearby sensitive receptors.

The proposed beverage grade ethanol modification has no significant sources of operational dust emissions. The proposed modifications listed in Section 3.11 include relocation of equipment, new tanks, a pipe, substation, cooling towers and a paved access road. The existing rail siding, which is being extended, is not a significant source of dust.

As dust impacts are only predicted to improve as a result of the proposed modifications, no modelling was undertaken. Shoalhaven Starches have existing dust controls in place to manage dust emissions at the site and impacts from the proposal are not expected at nearby sensitive receptors.

7. Dispersion modelling

The odour dispersion modelling was conducted using the US EPA regulatory Gaussian puff model CALPUFF Version 5.8. This model is also a recognised regulatory model in NSW. Where the modelling of odour dispersion is in complex terrain (as is the case at the Shoalhaven site), CALPUFF is recommended for use under NSW Guidelines. CALPUFF is especially suited for modelling light to calm wind conditions.

7.1 Model configuration and parameter selection

The following settings were used in the simulations:

- Model: CALPUFF Version 5.8
- The receptor grid was 25 km x 25 km, with a 200 m grid resolution
- The nearest receptors from the townships of Bomaderry (to the west) and Nowra (to the south) were used as sensitive receptors, along with a few isolated residences around the factory and environmental farm
- Ground level receptor heights have been modelled using the same terrain data as the
 original 2008 GHD assessment. This terrain data was used in the CALMET 2004 model
 which is used for CALPUFF modelling. In the June 2016 GHD Odour Audit, receptor
 heights were changed to represent latest available terrain data which is of higher
 resolution than the 2008 terrain data. This was identified as an error as the terrain in the
 corresponding CALMET model and CALPUFF model were not also updated. Receptor
 heights have therefore been reverted back to the original heights used in the 2008 model.
- Emissions were scaled based on a nose-response time for odour of one minute, applying a peak-to-mean ratio to the one hour average concentration of 2.3 for wake affected point sources and volume sources, and variable scaling for non-wake affected sources and area sources
- Meteorology was taken from the CALMET 2004 synthesised dataset, approved for use in previous studies.

7.2 Building wake effects

Building wake effects were modelled to the extent practicable. A summary of building heights input in to the model is provided below, with area sources shown in red and building footprints shown in grey. For proposed Scenario 1, additional buildings and structures were added to the southwest area of the factory.



Figure 8 Model setup for building wake effects – Existing and approved scenario (source: Lakes CALPUFF View, CALPUFF 3D 7.5.0)

7.3 Odour assessment

Table 7 shows the predicted odour levels for the existing situation and Scenario 1. Results of the mitigation scenario (change in the angle of the Gluten dryer 3 and 4 ducts) are also presented.

Figure 9 shows the predicted 99th percentile odour impacts (one minute nose-response time) for the existing and approved operations at the plant and environmental farm when compared to the incremental impact from the additional odour sources modelled in Scenario 1.

Figure 10 shows the predicted 99th percentile odour impacts (one minute nose-response time) for the existing and approved operations when compared to the incremental impact from the additional odour sources modelled in scenario 1 with mitigation.

Results show that the impact assessment odour criteria are achieved at R1 and R2 for both the existing scenario and Scenario 1, however exceeded at R3 and R4.

Results show that with the odour mitigation scenario, predicted odour levels achieve the impact assessment odour criteria at all receptors.

| | Range, | To nearest | | Odour | Odour impact, OU, 99 th percentile, nose-response time | | | | |
|----------------------|--------|------------------|-----------|-------|---|------------|---------------------------|--|--|
| Receptor | m | odour source | Direction | | Existing (Baseline) Scenario | Scenario 1 | Scenario 1 (Mitigated) | | |
| R1 Bomaderry | 150 | Packing Plant | W | 6 | 5 | 5 | 3 | | |
| R2 North Nowra | 1300 | Factory | SW | 3 | 3 | 3 | 2 | | |
| R3 Nowra | 700 | Factory | S | 5 | 6 | 6 | 4 | | |
| R4 Terara | 1300 | Factory | SE | 5 | 6 | 6 | 4 | | |

Table 7Predicted peak (99th percentile, short term averaged) odour impact
at nearby receptors





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Α 22 May 2017

Existing vs 'Mod 11 and Mod 12' (No mitigation)

Figure 9





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Job Number 21-26310 Revision Date

А 22 May 2017

Figure 10

Existing vs 'Mod 11 and Mod 12' (With mitigation)

8. Conclusions and implications

GHD was engaged by Manildra to conduct an air quality and odour impact assessment for a proposed modification to the approved SSEP.

The addition of the proposed sources of the DDG dryers requires the duplication of the two existing biofilters, taking the total number of on-site biofilters to four, in order to meet treatment requirements.

A marginal increase was observed in predicted odour impacts as a result of the addition of two biofilters, relocated cooling towers, the Mill feed silo and column washing vent when compared with existing operations plus those operations already approved. It is considered highly unlikely that this increase in odour would be detected at sensitive receptors.

As a result, it is predicted that no discernible increase in perceived odour impacts would be evident as a result of the proposed modifications to the plant. Odour modelling included the maximum measured quarter in regards to total odour levels from quarterly monitoring conducted at the EPA Licence points and is considered conservative.

Additionally, odour impacts were compared with previous odour assessments of the plant, with the following features observed from odour measurements and modelling results:

- An overall decrease in total odour emissions from the plant by around 12 % to the original ethanol expansion assessment in 2008.
- Odour impacts from Scenario 1 are similar to those predicted in 2008; with the exception of a slight extension of impacts to the south and south west, as a result of small changes to the layout of the plant and increases in emissions from Gluten Dryer Baghouse 3 and 4.
- An odour mitigations scenario has been undertaken which changes the angle that the Gluten Dryer Baghouse 3 and 4 duct release emissions. The mitigation scenario directs emissions towards vertical rather than horizontal and have been modelled with an increase stack exit velocity. This significantly increases dispersion and reduces predicted ground level odour impacts. Predicted odour levels with this mitigation scenario in place comply with the impact assessment criteria at all sensitive receptors, as shown in Table 7.

9. References

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Appendices

GHD | Report for Shoalhaven Starches Pty Ltd - Shoalhaven Starches expansion project - Modification 11 and Modification 12 (Project Approval MP_06_0228), 2126310 | 40 Appendix A – Meteorological analysis

The following section is taken from the Shoalhaven Starches Report on Ethanol Upgrade: Air Quality Assessment (GHD, 2008), and describes the meteorology of the area and how the dataset was compiled.

A1 Meteorology

The three-dimensional meteorological data for a CALPUFF model simulation are provided by CALMET₅, its meteorological pre-processor. CALMET requires meteorological input from surface weather station networks and upper air stations.

The following sub-sections describe the available meteorological data, how the data was applied and the features of the dispersion meteorological data used to run CALPUFF.

A1.1 Data Available

Wind data were collected at three locations within the Shoalhaven Starches facility. Of these three stations, only one station, the automated weather station (AWS) located near the storage ponds at the environmental farm (hereafter referred to as Farm AWS), is compliant with the Australian Standard for the measurement of horizontal wind for air quality applications (AS 2923:1987). The other two stations, in particular the weather station located at the factory, are compromised by building and equipment infrastructure. Wind data have been collected at the Farm AWS since 2003, with the most complete data set collected in 2004.

The nearest source of additional surface meteorological data was the Bureau of Meteorology (BoM) Nowra AWS located approximately 12 km to the west at the Royal Australian Navy base at Nowra (HMAS ALBATROSS). This data source was considered to be too far from the subject area to be site-representative.

The nearest source of upper air meteorological data was also the HMAS ALBATROSS site, which does irregular upper air soundings based on operational requirements. However, the time gap between these vertical atmospheric soundings is too large to be suitable for use as model input.

A1.2 Data Application

To take full advantage of the CALPUFF features, described in Section 7.1, and make use of the available meteorological data described above, a combined prognostic/diagnostic meteorological modelling approach was used to synthesise the three-dimensional meteorological data input required by CALPUFF.

The regional-scale prognostic meteorological model, TAPM₆, was used to simulate the meteorology over the subject site with consideration to the DECC *Approved Methods*. TAPM is an approved model for specialist applications and its use, as part of this assessment, is described in the next section.

The observations from the Farm AWS and Nowra AWS were first used for optimising and checking the performance of the prognostic model simulation.

Wind speed and wind direction data from the Farm AWS were then assimilated into the prognostic model.

The subsequent TAPM output (with assimilated Farm AWS data) was then passed to meteorological pre-processor model CALMET (version 5.5).

 ⁵ Scire J.S., E.M. Insley, R.J. Yamartino, and M.E. Fernau, 1995: A User's Guide for the CALMET Meteorological Model. Report prepared for the USDA Forest Service by EARTH TECH, Concord, MA. See: <u>http://www.src.com/calpuff/calpuff1.htm</u>
 ⁶ Hurley, P. The Air Pollution Model (TAPM) version 3. CSIRO Atmospheric Research Paper No. 31, 2005

A2 Prognostic Meteorological Modelling

TAPM (version 3.0.7) was developed at CSIRO Division of Atmospheric Research as a PCbased prognostic modelling system that can predict regional scale three-dimensional meteorology. TAPM accesses databases of synoptic weather analyses from the Bureau of Meteorology. The model then provides the link between the synoptic large-scale flows and local climatology, which includes characterising such factors as local land use and topography, and their influence on atmospheric stability and mixing height.

TAPM was initially configured with a nested model grid coverage designed to capture:

- Broad scale synoptic flows
- Regional to local scale wind channelling
- The influence of local land use

The nested grids were then configured with surface characteristics, such as terrain elevation, surface type (land use and vegetation type), soil type and deep soil moisture content.

Specific model settings were:

- Four nested grids at 1 000 m, 3 000 m, 10 000 m and 25 000 m resolution, with 55 x 55 grid points. The grid was set to ensure the locations of the Farm AWS and Nowra AWS were within the inner nested grid
- Surface vegetation and precipitation processes were included, whereas, non-hydrostatic processes were not included

Following an initial model run, the model output from the grid point nearest to the Farm AWS was compared with data recorded at that station. Specifically, the predicted hourly ambient temperatures and the annual wind rose (wind speed and direction distributions) were compared with corresponding recordings. Model output from the model grid point nearest to the Nowra AWS was also compared with an annual wind rose derived from data recorded at that station.

Figure A1 shows the scatter plot of observed and predicted ambient temperature at the Farm AWS. The determined optimal model configuration produced a correlation coefficient of 0.88 for predicted temperature. The strong correlation between predicted and recorded temperature indicates that the model is accurately calculating the surface energy balance, which, in turn, adds confidence to the hourly varying predictions made for atmospheric stability and the height of the mixed layer.





A2.1 Wind Distribution

Figure A2 shows the predicted (a) and observed (b) wind roses for the location of the Nowra AWS. The directional distribution of winds predicted by TAPM shows reasonable agreement with the recorded observations and with the wind patterns expected for this region.

Figure A3 shows the predicted (a) and observed (b) wind roses for the location of the Farm AWS after the initial TAPM simulation. The directional distribution of winds predicted by TAPM shows reasonable agreement with the recorded wind patterns expected for this region.

The wind speed and direction observations from the Farm AWS were assimilated into the prognostic model simulation to improve the ability of the model to capture the effects of local wind channelling and low wind speed conditions. The improvement to wind direction distributions in the model output is clearly evident in Figure A3(c). The marked improvement in the capture of low wind events is examined below.

It is understood that TAPM performs reasonably well at simulating low wind speeds when the atmosphere is unstable but is known to perform relatively poorly during stable atmospheric conditions⁷. This is a critical factor in this assessment given that odour emissions occur 24-hours per day, resulting in predictions of maximum odour impact dominating during these conditions.

Figure A4 shows a histogram of wind speed distribution for observations at the Farm AWS, predictions from TAPM and predictions from TAPM after wind speed and direction data from the Farm AWS were assimilated into TAPM. It is clear from this figure that TAPM did reasonably well at originally predicting moderate to high wind speeds but did relatively poorly predicting low wind speeds. However, Figure A4 also shows that the representation of low winds in the TAPM output was significantly improved once the Farm AWS data were assimilated into the model.

⁷ Luhar, A., Hurley, P. and Rayner, K. Improving Land Surface Processes in TAPM. Part 2: Low Wind Stable Conditions. 14th IUAPPA World Congress 2007



Figure A2 Nowra AWS - Annual Wind Roses (Year 2004)



Figure A3 Farm AWS - Annual Wind Roses (year 2004)



Figure A4 Wind Speed Distribution – TAPM and Farm AWS

To further investigate the effect of data assimilation on model output, a sensitivity analysis was conducted to compare the subsequent CALPUFF model predictions using meteorological input derived with and without the assimilation of observed wind speed and wind direction data from the Farm AWS into TAPM. Good agreement was found in the general pattern of dispersion (i.e. similar directions of poor dispersion), however, the highest ground level odour concentrations were predicted when the assimilated meteorological data file was used, which was expected given the higher frequency of light winds.

A3 Diagnostic Meteorological Model - CALMET

The TAPM output (with assimilated data) was then passed to model CALMET (version 5.5)⁸, which is the 3D meteorological diagnostic model pre-processor to the CALPUFF 3D puff based dispersion model.

Hourly varying 3D meteorological data, at a 1000 m resolution, were extracted from the TAPM inner nested grid and passed to CALMET in their entirety as initial guess fields. Surface meteorological parameters and vertical profile data were also extracted from TAPM at a grid point near the factory, and used as if they were observations in the diagnostic model (i.e. pseudo-data).

CALMET was configured with a 15 km by 15 km grid at 200 m resolution and with local scale surface characteristics, such as terrain elevation and land use (e.g. forest or sparse growth, water or residential). The land use and terrain elevation information was derived from US Geological Survey and AusLig data, respectively, with adjustments based upon inspection of aerial photographs, topographical and land uses maps, and a site inspection.

CALMET was used to produce hourly site-representative winds and micrometeorological information, which was used with the CALPUFF 3D puff-based dispersion model to assess the impacts of the air pollutants on the surrounding land uses.

⁸ Scire J.S., E.M. Insley, R.J. Yamartino, and M.E. Fernau, 1995: A User's Guide for the CALMET Meteorological Model. Report prepared for the USDA Forest Service by EARTH TECH, Concord, MA. See: <u>http://www.src.com/calpuff/.alpuff1.htm</u>

A3.1 Site-specific meteorology

Figure A5 shows a wind rose that illustrates the distribution of wind speed and direction at the location of the Factory. On an annual basis the prevailing winds are from the west with winds also from the west-north-west, north-west, west-south-west and north-east. The mean wind speed is 3.2 m/s, with higher speed winds associated with westerly winds with speeds up to 11 m/s; such speeds are not reached from other directions. The highest frequency of light winds occurs from the south-west, west and north.

Figure A6 provides a seasonal breakdown of the predicted wind distribution at the Factory, this figure reveals a north-easterly predominance during summer (sea-breeze) and a westerly predominance during the other seasons, in particular during winter.







Figure A6 Factory Seasonal Wind Roses - Year 2004

A categorised measure of atmospheric stability is also output from the model. These can be broadly defined as listed in Table A1.

| Stability Class | Description | Frequency of Occurrence ¹ |
|--------------------|--|---|
| A | Extremely unstable atmospheric conditions, occurring near the middle of day, with very light winds, no significant cloud. | 2% |
| В | Moderately unstable atmospheric conditions occurring during mid-morning/mid-afternoon with light winds or very light winds with significant cloud. | 14% |
| С | Slightly unstable atmospheric conditions occurring during early morning/late afternoon with moderate winds or lighter winds with significant cloud. | 17% |
| D | Neutral atmospheric conditions. Occur during the day or night with stronger winds. Or during periods of total cloud cover, or during twilight (transition) period. | 22% |
| E | Slightly stable atmospheric conditions occurring during the night-time with some cloud and/or light-moderate winds. | 12% |
| F | Moderately stable atmospheric conditions occurring during the night-time with no significant cloud and light winds. | 32% |

| Table A1 | Atmospheric Stabilit | y Classes and Distribution |
|----------|----------------------|----------------------------|
|----------|----------------------|----------------------------|

1. Stability data in this table extracted from Factory meteorological data

Potential off-site odour impact would tend to be maximised when winds are light and the atmosphere is stable, conditions that typically occur during the early evening and night-time. Table A1 shows that these conditions occurred for approximately 44% of the time.

The occurrence of stable air flows is of significance as these generally provide the conditions for worst case dispersion of emissions to air from ground based (or near-ground based) sources, and hence potentially the highest impact to odour amenity. This is due to the limited mixing in the vertical plane of these light wind airflows, and hence less dilution of the emissions from the majority of odour sources, which are either at ground level or wake affected short stacks. Therefore, the distribution of light wind stable flows can define the directions of "poor odour dispersion" from the factory and environmental farm.

Vertical mixing of airflows can be brought about by two mechanisms. The first is mechanical mixing caused by the shear stresses as air moves over rough terrain. The second is via thermal convective mixing, which has the potential to occur significantly only during daytime. The occurrence of unstable and strong-wind neutral air flows generally provide the conditions for the highest ground level concentrations due to emissions to air from elevated stack sources, such as the coal-fired boiler exhaust stacks found at the factory.

A rose that illustrates the directional distribution of the predicted atmospheric stability is shown in Figure A7. During these stable periods, the regional scale cool air drainage flows down the river valley from the west to dominate the transport and dispersion of emissions to air from the factory and environmental farm. To a lesser extent, local slope drainage flows from the elevated terrain located to the north, west-north-west and west-south-west of the site would also generate these conditions for poor dispersion.



Figure A7 Factory Annual Stability Rose - Year 2008

Appendix B - Complete odour emission inventory

The following Table details all sources modelled for both the existing and proposed modifications

| Source | EPA ID | ID | Source type | Height | Diameter | Exit velocity m/s | Exit temperature K | OER after control OUm³/s | Peak to mean adjusted total OER OUm³/s |
|---|-----------|--------|-------------------|---------|----------|----------------------|-----------------------|--------------------------------|---|
| Boiler No. 4 | 42 | BOILR4 | tall wake free | m 39 | m 1.1 | 1.7 | 417.2 | 3171.8 | var |
| Combined Boiler Stack for No. 5 & 6 Boilers. Coal combustion odour | 35 | BOILR5 | tall wake free | 54 | 2.05 | 13.5 | 411.2 | 38468.3 | var |
| additional cooling towers to the west (proposed) | | СТР | wake affected | 10 | 4.5 | 6 | 295 | 172.0 | 395.6 |
| Cooling towers | | DDG46 | wake affected | 10 | 4.5 | 6 | 295 | 172.0 | 395.6 |
| Light phase recovery tank | | DDG19 | wake affected | 11 | 0.1 | 3.3 | 362 | 20.0 | 46.0 |
| Pellet Mill Silo (proposed) | | PMFS | wake affected | 23 | | | | 173.0 | 397.9 |
| Pellet Plant exhaust stack | 46 | PPES | tall wake free | 49.2 | 1.5 | 14.1471061 | 318.2 | 38240.0 | var |
| Pellet silo (mill feed silo) | | S12 | wake affected | 2 | 0.3 | 0.1 | 304 | 350.0 | 805.0 |
| Stillage surge tank | | SST | wake affected | 2 | 0.2 | 3.3 | 360 | 149.0 | 342.7 |
| Vent condensor drain | | VCD | wake affected | 24.1 | 0.3 | 0.3 | 300 | 31.0 | 71.3 |

| Source | EPA ID | ID | Source type | Height m | Diameter m | Exit velocity m/s | Exit temperature K | OER after control OUm³/s | Peak to mean adjusted total OER OUm³/s |
|--|-----------|-------|-------------------------------|-------------|---------------|----------------------|-----------------------|--------------------------------|---|
| Ethanol Recovery Scrubber Discharge | 16 | ERESC | variable, wake affected | 28 | 0.3 | 7.1 | 299.5 | 2467.6 | 5675.5 |
| Fermenters (10-16) | 44 | FERM | tall wake free | 21 | 0.28 | 5.1 | 305.8 | 2667.5 | 6135.3 |
| Yeast propagators - tanks 4 & 5 | | YP45 | wake affected | 17 | 0.4 | 3.2 | 302 | 820.0 | 1886.0 |
| cyclone and fabric filter | | A4 | wake affected | 33 | 1.6 | 6 | 313 | 679.0 | 1561.7 |
| cyclone and fabric filter | | A5 | wake affected | 33 | 1.6 | 6 | 313 | 96.0 | 220.8 |
| cyclone and fabric filter | | A6 | wake affected | 33 | 1.6 | 6 | 311 | 449.0 | 1032.7 |
| cyclone and fabric filter | | A7 | wake affected | 33 | 0.8 | 9 | 297 | 932.0 | 2143.6 |
| Drum vacuum receiver | | C4 | wake affected | 21 | 0.2 | 20 | 314 | 1400.0 | 3220.0 |
| Dry gluten roof bin | | S07 | wake affected | 25 | 0.7 | 0.1 | 328 | 4500.0 | 10350.0 |
| Enzyme Tanks | | B7 | wake affected | 6 | 0.5 | 0.3 | 327 | 2042.0 | 4696.6 |
| Feed transfer to distillery | | E22 | wake affected | 15 | 0.3 | 0.1 | 300 | 83.0 | 190.9 |
| Flash Vessel Jet Cooker | | C1 | wake affected | 21 | 0.1 | 0.1 | 350 | 970.0 | 2231.0 |
| Flour bin aspirator | | S13A | wake affected | 2.5 | 0.4 | 0.1 | 306 | 500.0 | 1150.0 |
| Flour bin aspirator | | S13B | wake affected | 2.5 | 0.4 | 0.1 | 306 | 500.0 | 1150.0 |

| Source | EPA ID | ID | Source type | Height | Diameter | Exit velocity m/s | Exit temperature K | OER after control OUm³/s | Peak to mean adjusted total OER OUm³/s |
|--|-----------|------|---------------------------|--------|----------|----------------------|-----------------------|--------------------------------|---|
| Flour bin motor drive | | S06 | wake affected | 24 | 0.3 | 0.1 | 307 | 283.0 | 650.9 |
| Flour mill stack propsed and approved 1 | | FMP2 | wake affected | 31.8 | 0.68 | 4.4 | 320 | 266.0 | 611.8 |
| Flour mill stack propsed and approved 2 | | FMP1 | wake affected | 33.4 | 0.9 | 4.2 | 300 | 205.0 | 471.5 |
| Retention - tank 2 (now located in adjacent tank) | | GRT | wake affected | 21 | 0.25 | 0.1 | 293 | 3250.0 | 7475.0 |
| High protein dust collector | | S08 | wake affected | 24.5 | 0.4 | 0.1 | 316 | 600.0 | 1380.0 |
| Incondensible gases vent | | D6 | wake affected | 13 | 0.2 | 0.6 | 309 | 558.0 | 1283.4 |
| lon exchange effluent tank | | C18 | wake affected | 2.5 | 0.32 | 0.1 | 307 | 250.0 | 575.0 |
| Jet cooker 1 - retention tank | | E13 | wake affected | 10 | 0.2 | 0.1 | 362 | 1067.0 | 2454.1 |
| Jet cooker 2 & 4 - Retention | | E7 | wake affected | 9 | 0.1 | 2.2 | 373 | 567.0 | 1304.1 |
| Molecular Sieve - Vacuum drum | | D2 | wake affected | 10 | 0.1 | 13 | 337 | 1350.0 | 3105.0 |
| No. 1 Gluten Dryer baghouse | 8 | S02 | wake affected point | 25.5 | 3.2 | 0.1 | 344.7 | 5925.0 | 13627.5 |

| Source | EPA ID | ID | Source type | Height | Diameter | Exit velocity m/s | Exit temperature K | OER after control OUm³/s | Peak to mean adjusted total OER OUm³/s |
|--|-----------|------|------------------|--------|----------|---------------------------|-----------------------|--------------------------------|---|
| No. 1 Starch Dryer | 12 | S01 | wake affected | 26 | 1.3 | 9.3 | 314.2 | 5193.3 | 11944.7 |
| No. 2 Gluten Dryer baghouse (aka. No 2 Starch Dryer) | 9 | S04 | wake affected | 27 | 3.2 | 0.1 | 333.2 | 2353.7 | 5413.4 |
| No. 3 Gluten Dryer baghouse | 10 | S03 | wake affected | 21 | 2.5 | 0.1 (9.95 mitigation) | 348.2 | 58916.7 | 135508.3 |
| No. 3 Starch Dryer | 13 | S18 | wake affected | 20 | 1.2 | 21.8 | 317.2 | 1663.2 | 3825.4 |
| No. 4 Gluten Dryer baghouse | 11 | S05 | wake affected | 30 | 2.7 | 0.1 (11.72 mitigation) | 349.2 | 31221.7 | 71809.8 |
| No. 4 Starch Dryer | 14 | S19 | wake affected | 20 | 1.2 | 21.8 | 315.7 | 1824.0 | 4195.2 |
| No. 5 Ring Dryer Starch | | SDR5 | wake affected | 25 | 1.2 | 0.1 | 320 | 4817.0 | 11079.1 |
| No. 5 Starch Dryer | | SD5 | wake affected | 33.5 | 2.35 | 14.96 | 329.2 | 6800.0 | 15640.0 |
| No. 6 Gluten Dryer | | GD6 | wake affected | 35 | 1.7 | 22.4 | 346.2 | 12568.0 | 28906.4 |
| No. 7 Gluten Dryer | | GD7 | wake affected | 29 | 1.7 | 18.9 | 341.2 | 9553.0 | 21971.9 |
| Spray dryer | | S20 | wake affected | 19 | 1.4 | 0.1 | 335 | 738.0 | 1697.4 |
| Starch factory rejects collection tank | | E10 | wake affected | 8 | 0.1 | 0.1 | 308 | 183.0 | 420.9 |

| Source | EPA ID | ID | Source type | Height m | Diameter m | Exit velocity m/s | Exit temperature K | OER after control OUm³/s | Peak to mean adjusted total OER OUm³/s |
|-------------------------|-----------|------|------------------|-------------|---------------|----------------------|-----------------------|--------------------------------|---|
| Large Starch Silo 1 | | PPL1 | wake affected | 26.5 | 0.16 | 6.8 | 323.2 | 86.4 | 198.8 |
| Large Starch Silo 2 | | PPL2 | wake affected | 26.5 | 0.16 | 6.8 | 323.2 | 86.4 | 198.8 |
| Medium Gluten Silo 1 | | PPM1 | wake affected | 20.7 | 0.16 | 6.8 | 323.2 | 173.0 | 397.9 |
| Medium Gluten Silo 2 | | PPM2 | wake affected | 20.7 | 0.16 | 6.8 | 323.2 | 173.0 | 397.9 |
| Medium Gluten Silo 3 | | PPM3 | wake affected | 20.7 | 0.16 | 6.8 | 323.2 | 173.0 | 397.9 |
| Small Gluten Silo | | PPS1 | wake affected | 34.3 | 0.2 | 18.6 | 323.2 | 91.6 | 210.6 |
| Small Starch Silo | | PPS2 | wake affected | 34.3 | 0.2 | 18.6 | 323.2 | 35.0 | 80.5 |
| Biofilter A | 40 | BIO1 | area | | | | | 440.0 | var |
| Biofilter B | 41 | BIO2 | area | | | | | 330.0 | var |
| Biofilter C | | BIO3 | area | | | | | 1089.0 | |
| Biofilter D | | BIO4 | area | | | | | 1280.0 | |
| Effluent storage dam 1 | 19 | PO1 | area | | | | | 147.5 | var |
| Effluent storage dam 2 | 20 | PO2 | area | | | | | 1656.4 | var |
| Effluent storage dam 3 | 21 | PO3 | area | | | | | 191.7 | var |
| Effluent storage dam 5 | 23 | PO5 | area | | | | | 515.2 | var |

| Source | EPA ID | ID | Source type | Height | Diameter | Exit velocity m/s | Exit temperature K | OER after control OUm³/s | Peak to mean adjusted total OER OUm³/s |
|--|-----------|-------|------------------|--------|----------|----------------------|-----------------------|--------------------------------|---|
| Effluent storage dam 6 | 24 | PO6 | area | | | | | 1775.3 | var |
| Sulphur Oxidisation Basin | 25 | SOBAS | area | | | | | 829.8 | var |
| Membrane bio- reactor | | MBR | wake affected | | | | | 62.4 | |
| DDG load out shed - awning | | DDG35 | volume | | | | | 923.0 | 2122.9 |
| DDG product storage sheds | | DDG34 | volume | | | | | 1023.0 | 2352.9 |
| DDG tent storage area | | DDG36 | volume | | | | | 1929.0 | 4436.7 |
| Pellet plant fugitives (discharged direct to atmosphere) | | PPF | wake affected | | | | | 5771.0 | 13273.3 |
| Farm tank | | F18 | volume | | | | | 3834.0 | 8818.2 |
| Column washing vent | | CWV | point | | | | | 23.3 | 53.6 |
| Flour Mill B (proposed, pending approval) | | FMBA | point | 39.5 | 0.65 | 10.1 | 322 | 560.0 | 1288.0 |
| Flour Mill B (proposed, pending approval) | | FMBB | point | 39.5 | 1 | 9.55 | 322 | 1260.0 | 2898.0 |

| Source | EPA ID | ID | Source type | Height m | Diameter m | Exit velocity m/s | Exit temperature K | OER after control OUm³/s | Peak to mean adjusted total OER OUm³/s |
|--|-----------|------|----------------|-------------|---------------|----------------------|-----------------------|--------------------------------|---|
| Flour Mill B (proposed, pending approval) | | FMBC | point | 39.5 | 1 | 9.55 | 322 | 1260.0 | 2898.0 |
| Flour Mill B (proposed, pending approval) | | FMBD | point | 39.5 | 0.65 | 10.1 | 300 | 257.0 | 591.1 |
| Flour Mill B (proposed, pending approval) | | FMBE | point | 39.5 | 1.1 | 8.77 | 300 | 642.0 | 1476.6 |
| Flour Mill B (proposed, pending approval) | | FMBF | point | 39.5 | 1.1 | 8.77 | 300 | 642.0 | 1476.6 |
| Flour Mill B (proposed, pending approval) | | FMBG | point | 39.5 | 0.5 | 10.2 | 293 | 200.0 | 460.0 |
| Flour Mill B (proposed, pending approval) | | FMBH | point | 39.5 | 0.65 | 9.04 | 293 | 300.0 | 690.0 |
| Flour Mill B (proposed, pending approval) | | FMBI | point | 39.5 | 0.65 | 9.04 | 293 | 300.0 | 690.0 |
| Flour Mill B (proposed, pending approval) | | FMBM | point | 24 | 0.65 | 6.53 | 294 | 217.0 | 499.1 |



Appendix C – Summary of quarterly EPA Licence Point odour emissions

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35164/https://projects.ghd.com/oc/Sydney/manildramod13airqual/Delivery/Documents/2126310-REP-A_Manildra_Mod11_12_Rev0.docx

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